Chem 531: Problem Set #1 **SOLUTIONS**

- **(1)**
- (a) Calculate $q, w, \Delta U$, and ΔH for the reversible isothermal expansion at 300 K of 5.00 mol of an ideal gas from 500 to 1500 cm³.
- (b) What would ΔU and w be if the expansion connects the same initial and final states as in (a) but is done by having the ideal gas expand into vacuum?
- (c) Likewise, if the gas expands against a constant pressure of 10 bar, how much work is done by the gas?
- (suthermal, so DU= DH= O for an ideal gas

W= - [PdV since reversible

 $=-(5.30)(8.3145)(300) ln \frac{730}{1500} = -13732 J$

=-13.7 RJ

DU=0= 3+W, so g=+13.7 25

free expansion: W=-SPextdV = 0 smile Pext=0

Still is othernal, so DU=DH=O but now g=0 too

(C) const pressure expansion: W=- [Pext dV = - Pext dV

W= - Pext DV 2 this is work done on the gas

Work done by the gas is + Pext DV

W= (10 bar) + 10 Pc x (1500-500) x (1500-500)

= +1000 T = +1.0 RJ

(2) A nearly flat bicycle tire becomes noticeably warmer after it has been pumped up. Approximate this process as a reversible adiabatic compression. Assume the initial pressure and temperature of the air before it is put into the tire to be $P_i = 1.00$ bar and $T_i = 298$ K. The final volume of the air in the tire is $V_f = 1.00$ L and the final pressure is $P_f = 5.00$ bar. Calculate the final temperature of the air in the tire. Assume that $\overline{C}_v = 5R/2$.

go ahead and start us
$$\left(\frac{T_{f}}{T_{h}}\right) = \left(\frac{V_{f}}{V_{h}}\right)^{-R/C_{h}}$$

$$\left(\frac{V_{f}}{V_{h}}\right) = \frac{NRT_{f}}{P_{f}} = \left(\frac{T_{f}}{T_{h}}\right) \left(\frac{P_{h}}{P_{f}}\right)$$

$$So \left(\frac{T_{f}}{T_{h}}\right) = \left(\frac{P_{h}}{T_{h}}\right)^{-R/C_{h}}$$

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- (3) For a certain ideal gas, $\bar{C}_v = 2.5 \text{R}$ at all temperatures. Calculate $q, w, \Delta U$, and ΔH when 2.00 mol of this gas undergoes each of the following processes:
- (a) a reversible isobaric expansion from (1.00 atm, 20.0 L) to (1.00 atm, 40.0 L)
- (b) a reversible isochoric change of state from (1.00 atm, 40.0 L) to (0.500 atm, 40.0 L)
- (c) a reversible isothermal compression from (0.500 atm, 40.0 L) to (1.00 atm, 20.0 L). Also calculate q, w, ΔU , and ΔH for the cycle that consists of steps (a), (b), and (c).

note: I'm going to use L-atm units for energy in this problem

a) $W = -\int PAV = -PAV$ since isobaric o reversible = -(1.50 otm)(20.0 L) = -200 L-atm

DU = SCV dT since it's on ideal gus

= $(2.00 \,\text{mel})(2.5 \,\text{R})(T_f - T_i)$ $T_f = \frac{P_f V_f}{nR} = \frac{(1.00)(40.0)}{(2.00)(0.08206)}$ = $243.7 \,\text{K}$

likevisé, 1/2 121.9 12

00 Du= 50.0 L-atm

g = DU-W = 50,0 - (-20,0) = 70,0 L-ctm

DH = DU + D(PV) = DU + P DV (1suboric)

= 20.0 + (1.00)(20.0)

= 70.0 L-atm = gp

(b) Isocheric 1.00 atm
$$\rightarrow$$
 0.500 atm @ 40.0 L
 $T_{1} = \frac{P_{1}V_{1}}{nR} = \frac{(1.00)(40.0)}{(2.50)(0.08706)} = 243.7 \text{ K}$

$$\Delta U = g_v = \int C_v d\tau = (2.00)(2.5 R)(-121.8)$$

= -50.0 L-atm

$$\Delta H = \Delta U + \Delta (PV) = \Delta U + V \Delta P$$

$$= -50.0 + (40.0)(0.500 - 1.00)$$

$$= -70.0 L - etm$$

$$\Delta U = \Delta H = 0$$
 since ideal gas + isothernal
$$\beta = -W \quad \Leftrightarrow \quad \omega = -\int PdV = -nRT \int_{V}^{dV} = -nRT \ln \frac{Vf}{Vf}$$

$$= -(2.00)(0.08206)(121.9) \ln \frac{20.0}{40.0}$$

$$\psi = 13.9 \text{ L-atm}$$

$$g = -13.9 \text{ L-atm}$$

a cycle:
$$a \rightarrow b \rightarrow c$$
 $g = 70.0 + (-13.0) + (-13.9) = 6.10 Leath$
 $0 = -20.0 + 0 + 13.9 = -6.10 Leath$
 $0 = -20.0 + 0 + 13.9 = -6.10 Leath$

- (a) Starting with the total differential of P as a function of V and T, obtain an expression for ΔP in terms of α (thermal expansion coefficient) and κ (isothermal compressibility) for the situation where both the temperature and volume change in a general process. Show all work.
- (b) A <u>rigid</u> container is filled completely with liquid water and sealed at 25.0°C and a pressure of 1.00 bar. What is the final pressure if the temperature of the system is raised to 60.0°C? Under these conditions $\alpha_{water} = 2.04 \times 10^{-4} \text{ K}^{-1}$ and $\kappa_{water} = 4.59 \times 10^{-5} \text{ bar}^{-1}$ are constants. (Note: α is not really a constant it rises to 5.16 x 10⁻⁴ K⁻¹ at 60°C but don't worry about that for this problem)

$$\begin{array}{ll}
\text{all} & P = P(V,T) & dP = \left(\frac{\partial P}{\partial V}\right)_{T} dV + \left(\frac{\partial P}{\partial T}\right)_{V} dT \\
\text{but} & 2 = \frac{1}{V}\left(\frac{\partial V}{\partial T}\right)_{P} & \text{all} & \mathcal{X} = -\frac{1}{V}\left(\frac{\partial V}{\partial P}\right)_{T} \\
\text{all} & \left(\frac{\partial P}{\partial T}\right)_{V} = \frac{2}{\mathcal{X}}
\end{array}$$

hence
$$dP = \frac{-1}{VK}dV + \frac{2}{K}dT$$

$$\Delta P = -\frac{1}{VK}dV + \frac{2}{K}dT$$

$$\Delta P = -\frac{1}{VK}dV + \frac{2}{K}dT$$

D for a rigid container, dV=D, so $\Delta P=\int_{-T_{c}}^{+} dT$

assuming T independence of 2 and R,

$$\Delta P = \frac{2.04 \times 10^{-4}}{4.59 \times 10^{-5}} (60.0 - 25.0) = 156 \text{ ber}$$

(5) Calculate the molar heat of vaporization of water at 25°C. The heat of vaporization of water at 100°C is 40.68 kJ/mol.

$$H_2O(R)$$
 $\xrightarrow{\Delta H_{vop}(25\tilde{c})}$ $H_2O(5)$ $25^{\circ}C$ ΔH_1 ΔH_2 $\Delta H_{vop}(150\tilde{c})$ $H_2O(8)$ $\Delta H_2O(8)$ $\Delta H_2O(8)$

$$\Delta H_{vap} (25^{\circ}C) = \Delta H_1 + \Delta H_{vap} (100^{\circ}C) + \Delta H_2$$

$$\Delta H_1 = \int C_p (1420(a)) dT = (75.3) (100-25) = 5647 J/ml$$
25

$$DH_2 = \int_{100}^{25} C_p(H_2O(97)) dT = (33.6)(25-100) = -2520 J/ml$$